熱力を告 熱力からから 人を疑10分>

- 1. 清畫世P-V diagram for a Carnot power cycle executed by a gas, 並稍作这明。
- 2. 鸟出 Cv, G, 印建义。

$$C_{N}=\frac{\partial()}{\partial T}$$
), $C_{P}=\frac{2()}{\partial T}$, $C_{P}=\frac{2()}{\partial T}$), $C_{P}=\frac{2()}{\partial T}$, $C_{P}=\frac{2()}{\partial T}$), $C_{P}=\frac{2()}{\partial T}$, $C_{P}=\frac{2()$

- 3. if a refrigeration cycle \$12 a heat pump cycle \$8 coefficient of performence 有何 不同。
- 4. 清畫出 Temperature-entropy diagram of the ideal Rankine cycle, 五特作記明.
- 5. 9 & specific Gibbs function, jt July dg = ordp - sdT

元智機械研究所博士班資格考 911 熱傳試題

- (15%) Define the following no-dimensional parameters, then describe their physical meanings. (Such as force ratio, property ratio ect.)
 - (a). Reynolds number (Re), (b). Prandtl number (Pr), (c). Nusselt number(Nu), (d). Grashof number (Gr), (e). Weber number (We)
- 2. (20%) One of the few situation for which exact solution to the convection transfer equations may be obtained involve what is termed parallel flow. In this case fluid motion is only in one direction. Consider a special case of parallel flow involving stationary and moving plates of infinite extent separated by a distance L, which intervening space filled by an incompressible fluid. This situation is referred to as Coutte flow and occurs, for example, in a journal bearing.
 - (1). What is appropriate form of the continuity equation, reduced from eq. 1
- (2). Beginning with the momentum equation 2, simplified the equation, at given boundary condition and determine the velocity distribution between the plates
- (3). Beginning with the energy equation 3, simplified the equation, at given boundary condition and determine the temperature distribution between the plates.

$$\begin{split} &\frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} = 0 \quad eq. \ 1 \\ &\rho \bigg(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \bigg) = -\frac{\partial p}{\partial x} + \frac{\partial}{\partial x} \bigg\{ \mu \bigg[2 \frac{\partial u}{\partial x} - \frac{2}{3} \bigg(\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} \bigg) \bigg] \bigg\} + \frac{\partial}{\partial y} \bigg[\mu \bigg(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \bigg) \bigg] + X \quad eq. 2 \\ &\rho c_p \bigg(u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \bigg) = \frac{\partial}{\partial x} \bigg(k \frac{\partial T}{\partial x} \bigg) + \frac{\partial}{\partial y} \bigg(k \frac{\partial T}{\partial y} \bigg) + \mu \Phi + \dot{q} \quad eq. 3 \end{split}$$

- (15%) Consider flow in a circular tube. Within the test section length(between 1 and 2) a constant heat flux q_s is maintained.
 - (a). For the two cases identified sketch, qualitatively, the surface temperature T_S(x) and the fluid meam temperature T_m(x) as a function of distance along the test section x. In case A flow is hydrodynamically and thermally fully developed. In case B flow is not developed.
 - (b). Assuming that the surface flux q_s and the inlet mean temperature $T_{m,1}$ are identical for both cases, will the exit mean temperature $T_{m,2}$ for caseA be greater, equal to, or less than $T_{m,2}$ for case B? Briefly explain why.

